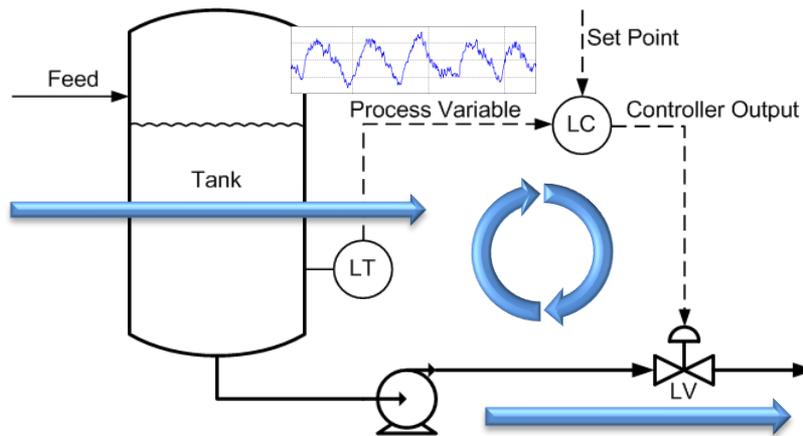


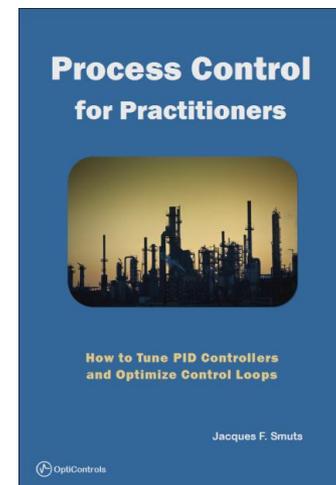
Analyzing Control Problems and Improving Control Loop Performance

-by Jacques F. Smuts



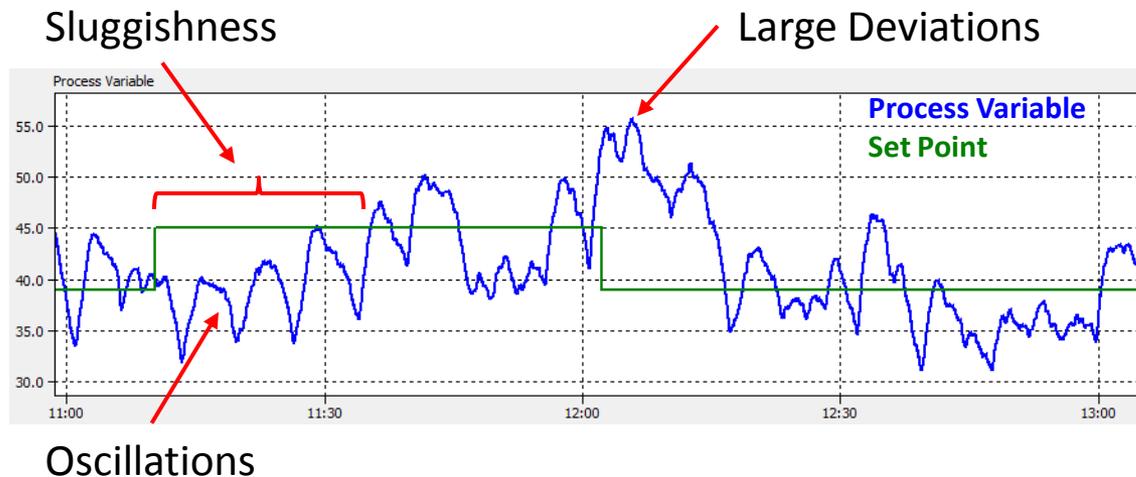
CHEM|INNOVATIONS
2011 | CONFERENCE
& EXPO

- ▶ Principal Consultant at OptiControls Inc.
 - League City, TX
- ▶ 20 years experience in process control
 - Loop optimization and troubleshooting
 - Consulting and control strategy design
 - Process control training
- ▶ Senior member of ISA, P.E., Ph.D.
- ▶ Author of the book:
“Process Control for Practitioners”

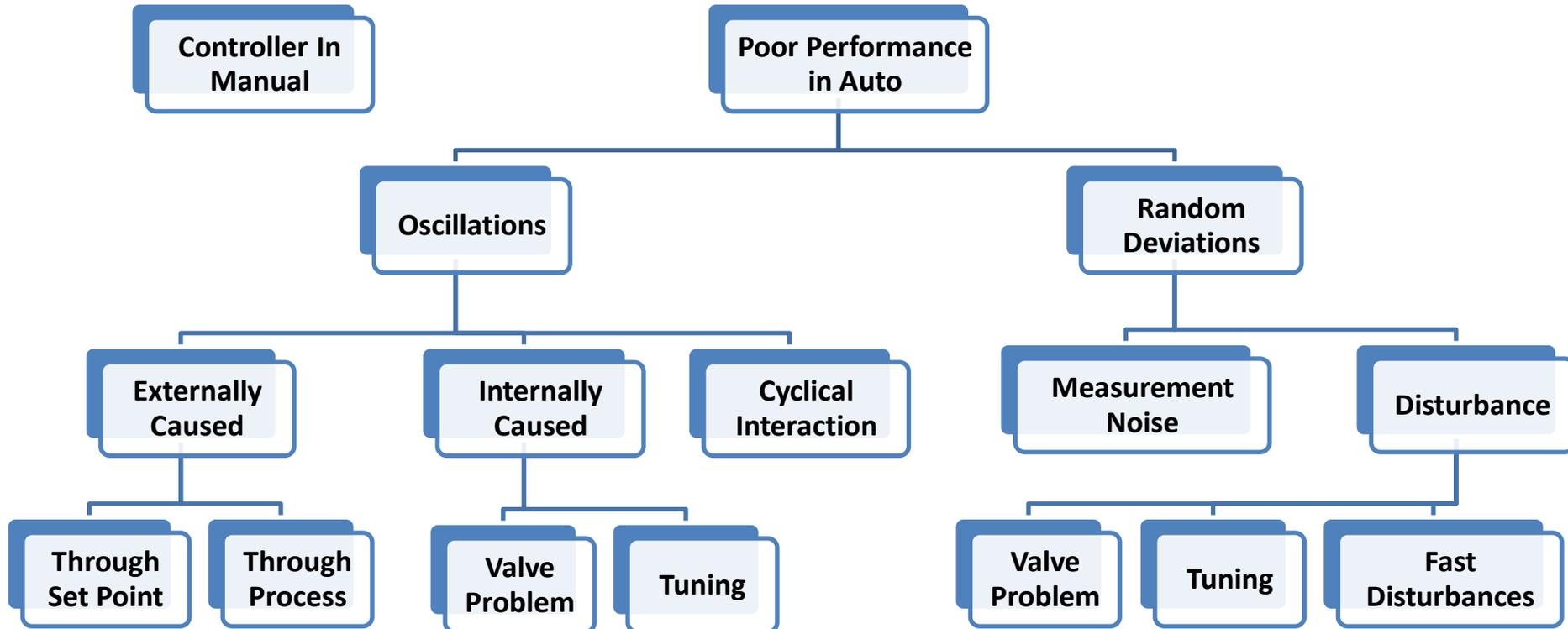


Poor Loop Performance

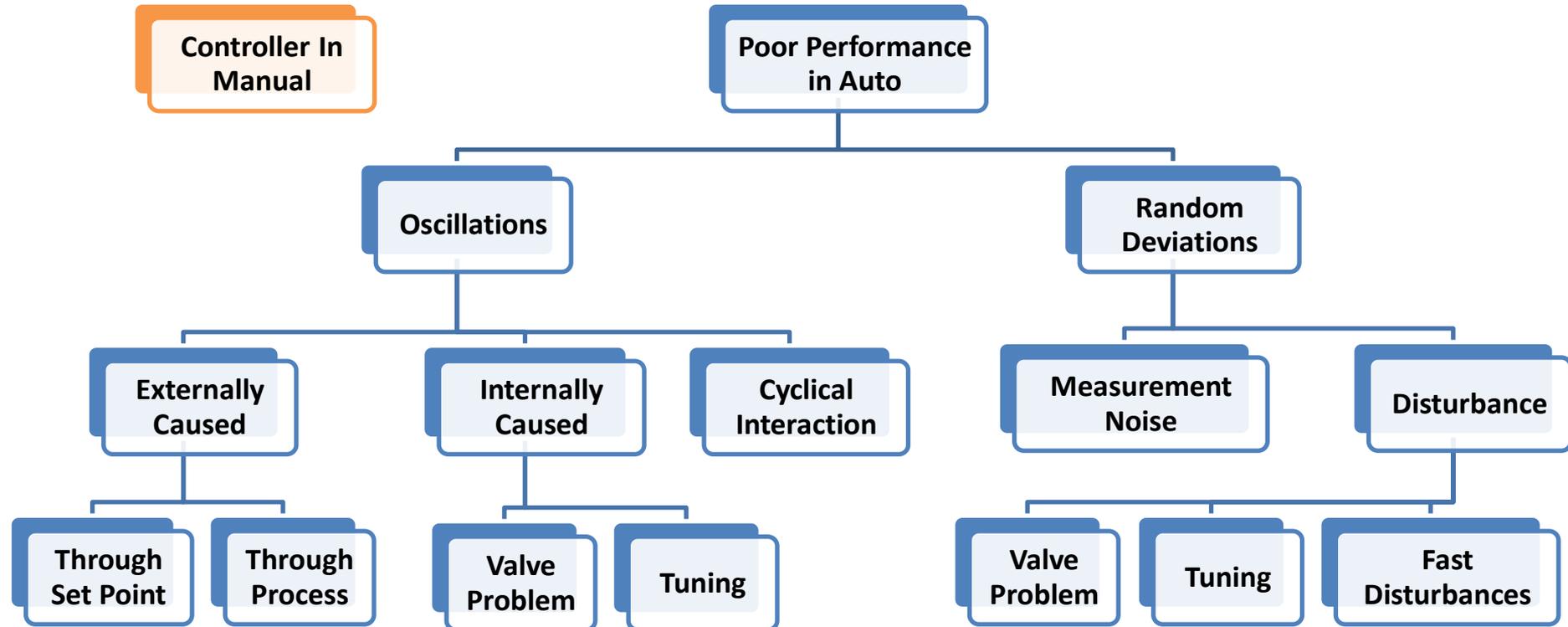
- ▶ Loop is in manual
- ▶ Poor performance in auto
 - Loop oscillates or goes unstable
 - Sluggish and/or large deviations from set point
- ▶ Often not tuning related



Problem Analysis

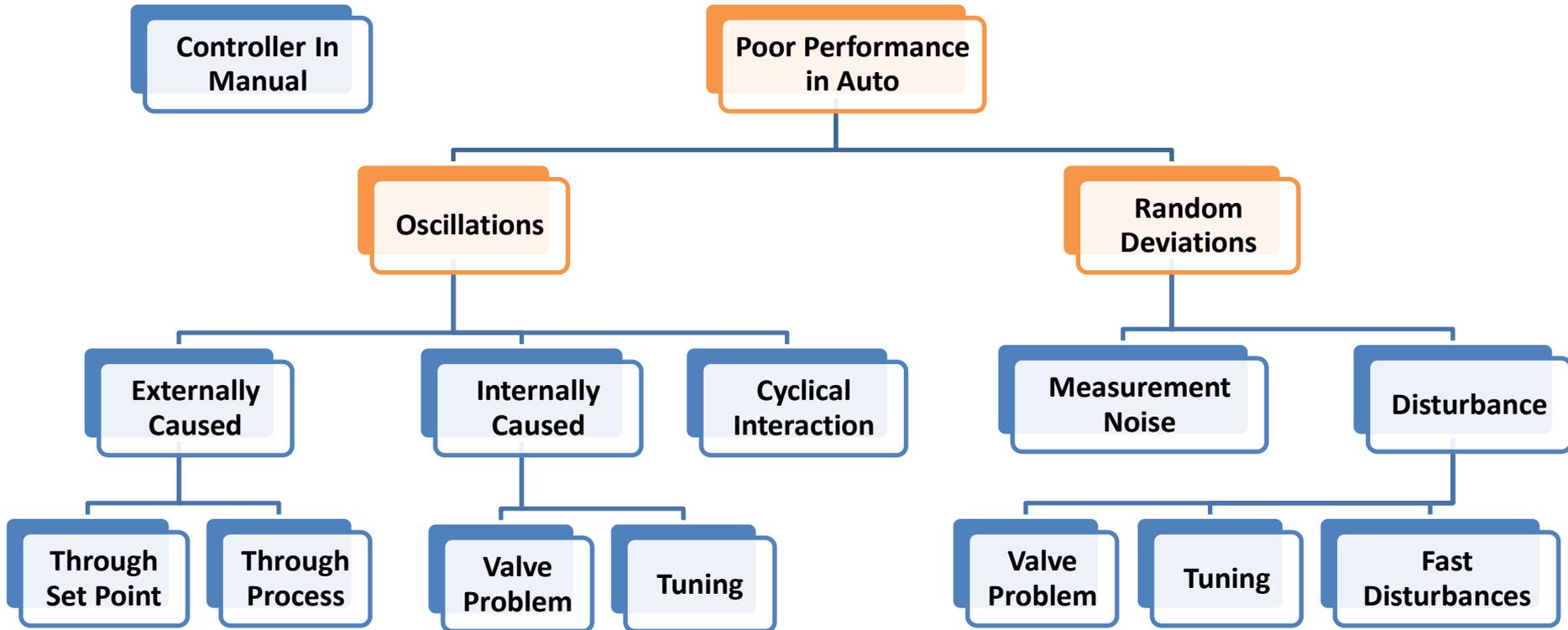


Problem Analysis



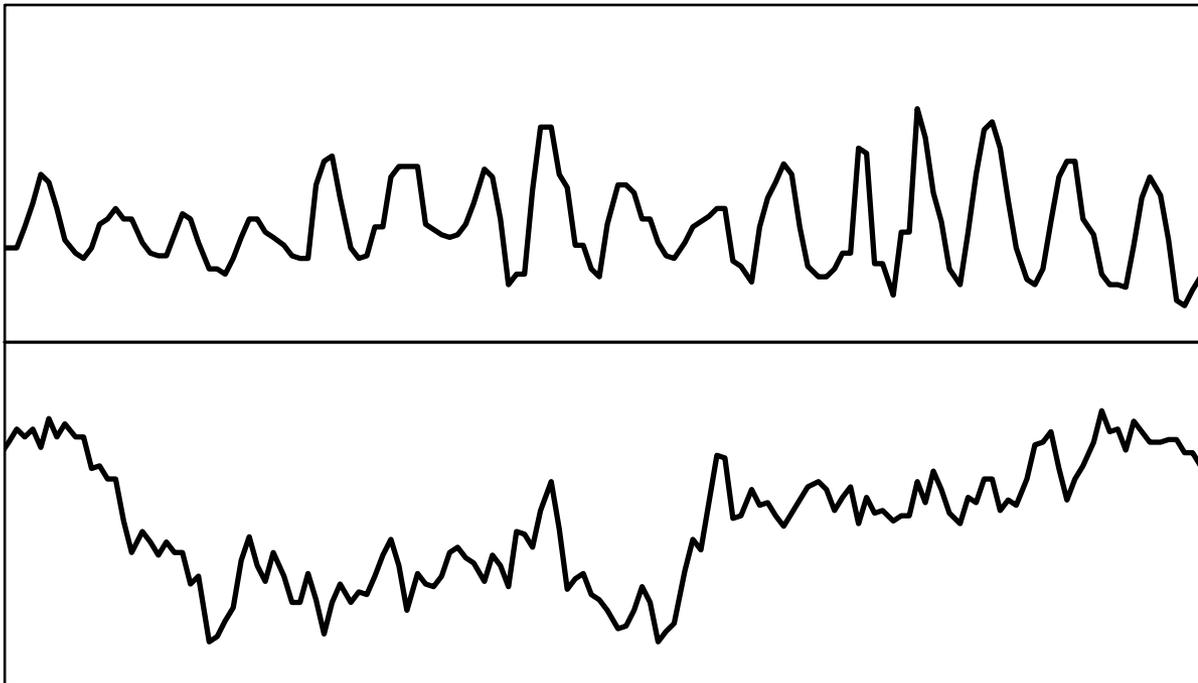
- ▶ Some loops: Okay to be in manual
 - Redundant, standby equipment
 - Certain process modes
- ▶ All other loops should be in auto
 - Check reason for manual with operator
 - Review historical performance
 - Place in automatic mode to see response

Problem Analysis



Cyclical or Random

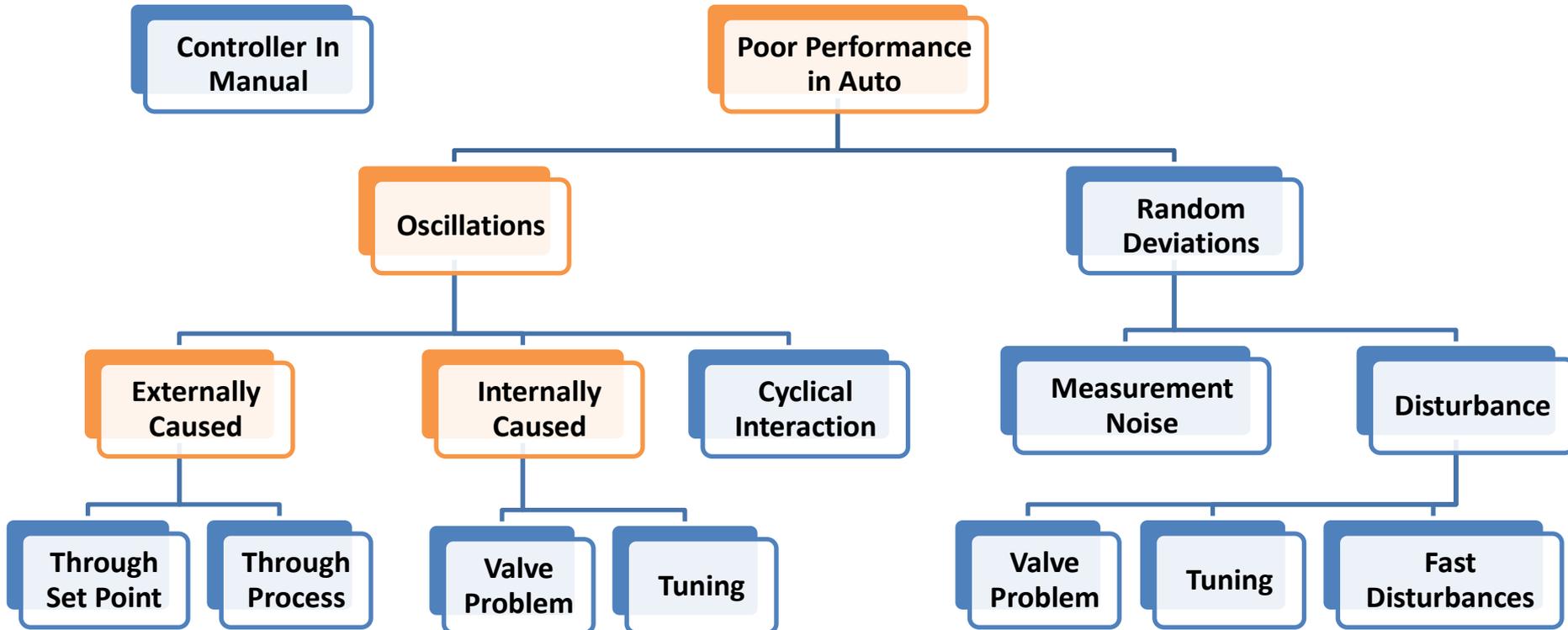
- ▶ Analyze process variable to determine
 - Visually
 - Use frequency analysis software



Oscillations have a repeatable, constant period

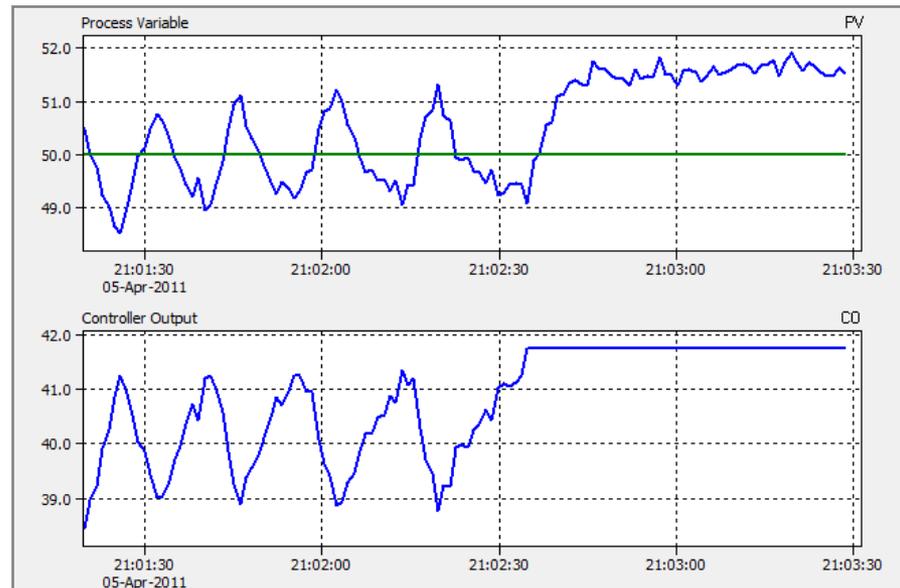
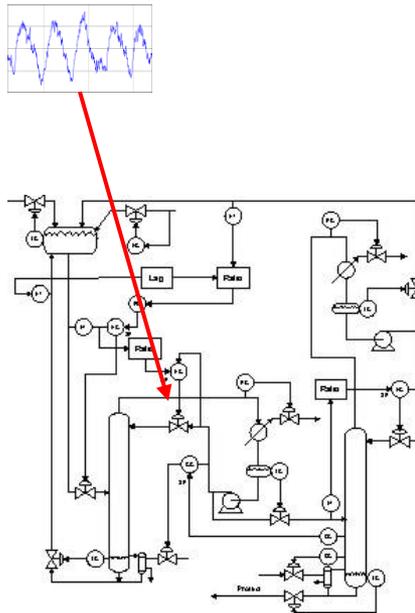
Noise and disturbances are random

Problem Analysis

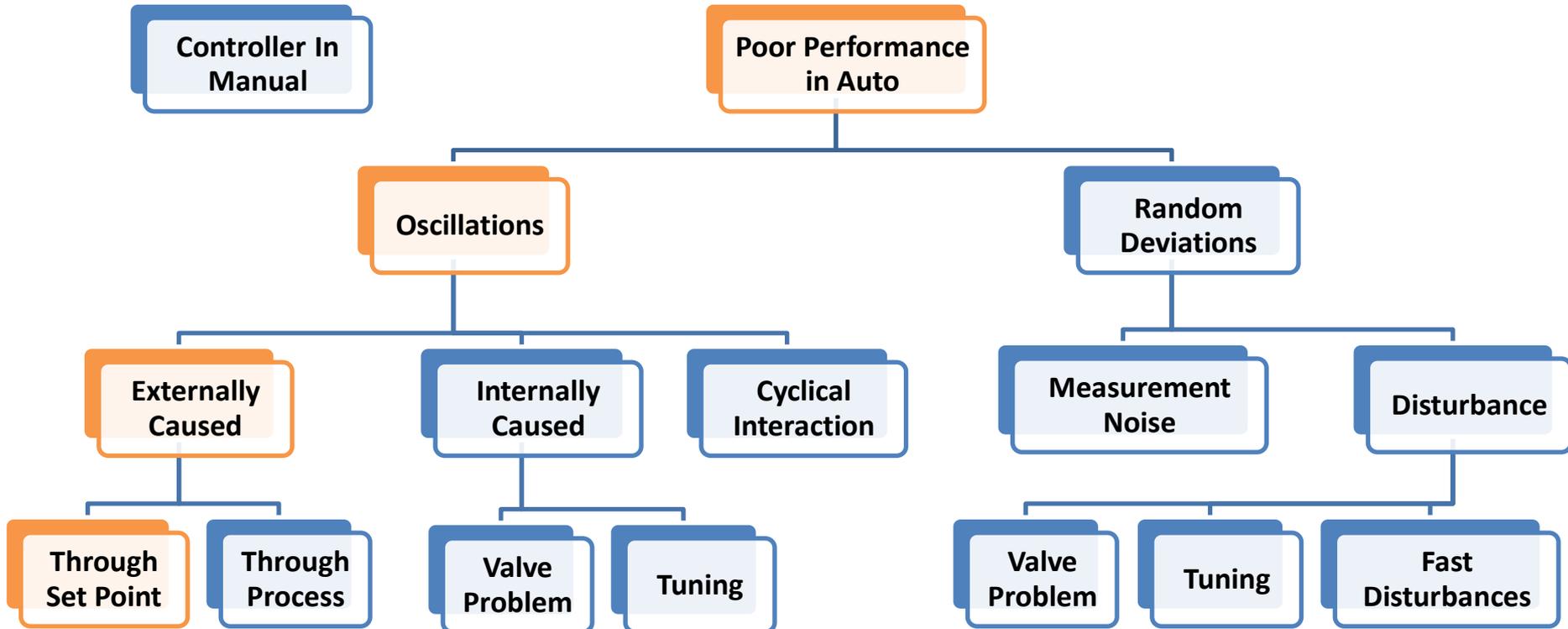


Internal vs. External Oscillations

- ▶ Diagnostic Test: Place loop in manual
- ▶ PV continues to oscillate \Rightarrow external source
- ▶ Oscillation ceases \Rightarrow internal problem

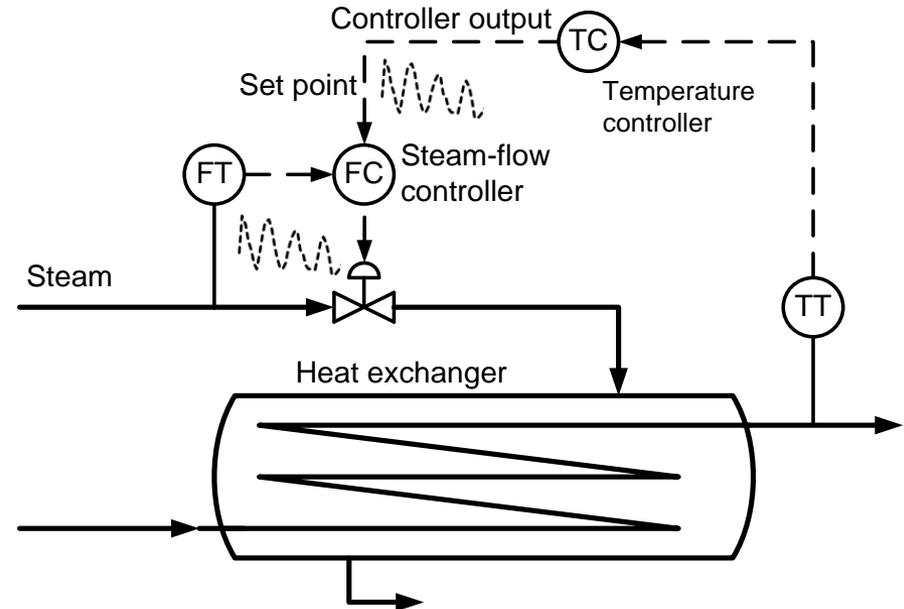


Problem Analysis

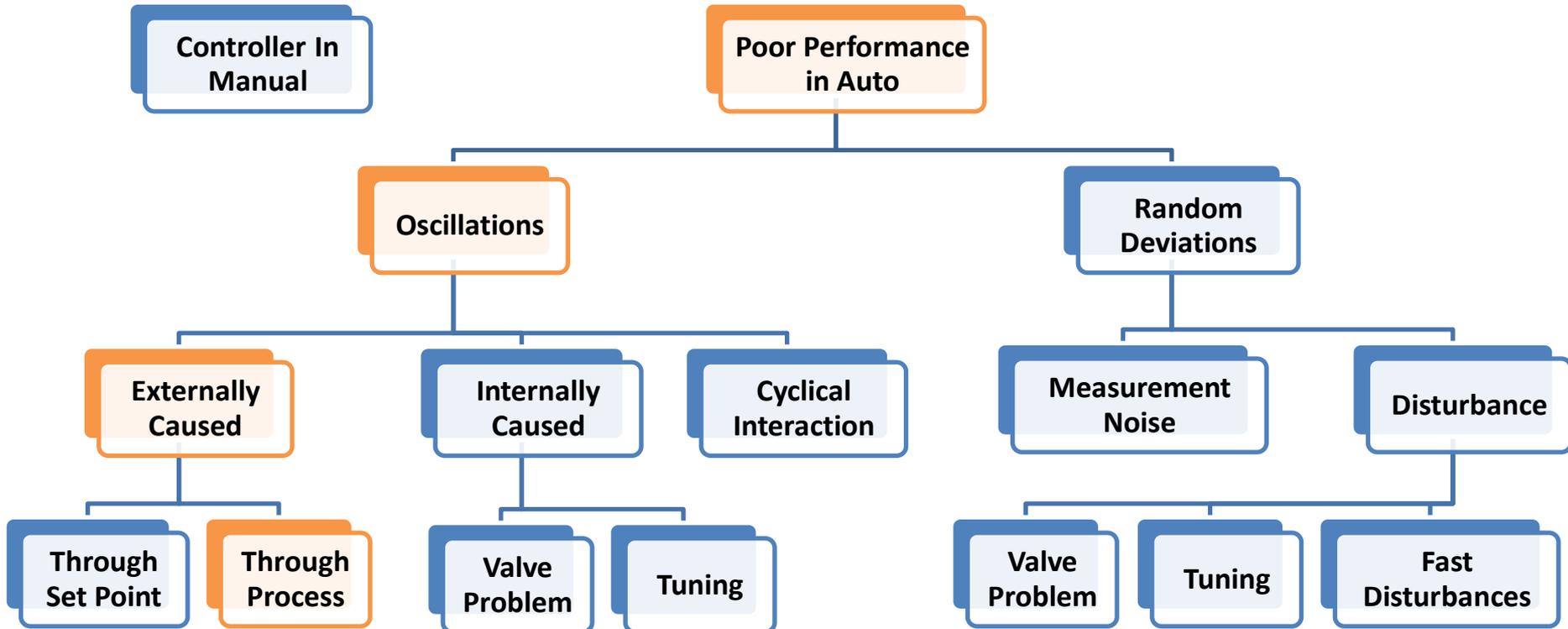


Oscillating Set Point

- ▶ E.g. steam flow loop oscillates and its set point oscillates
- ▶ Place temperature loop in manual
 - Flow loop stops oscillating: analyze temperature loop
 - Flow loop still oscillates: analyze flow loop

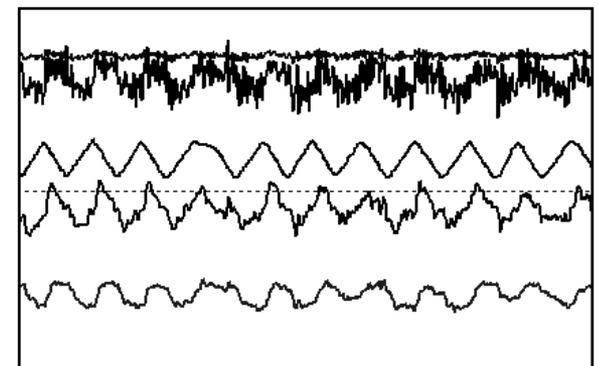
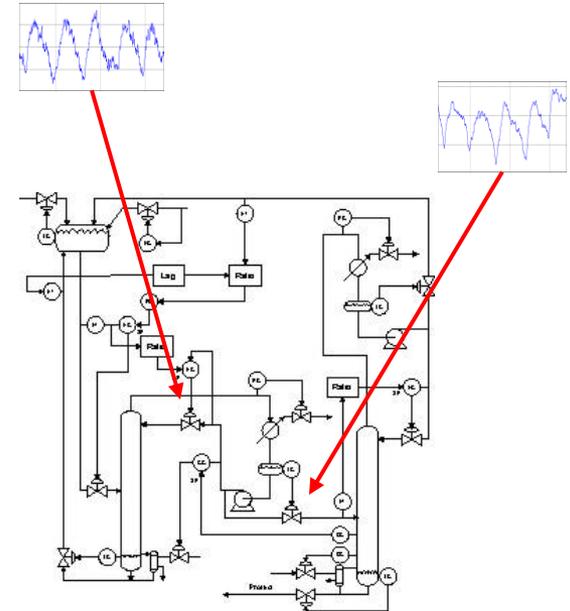


Problem Analysis

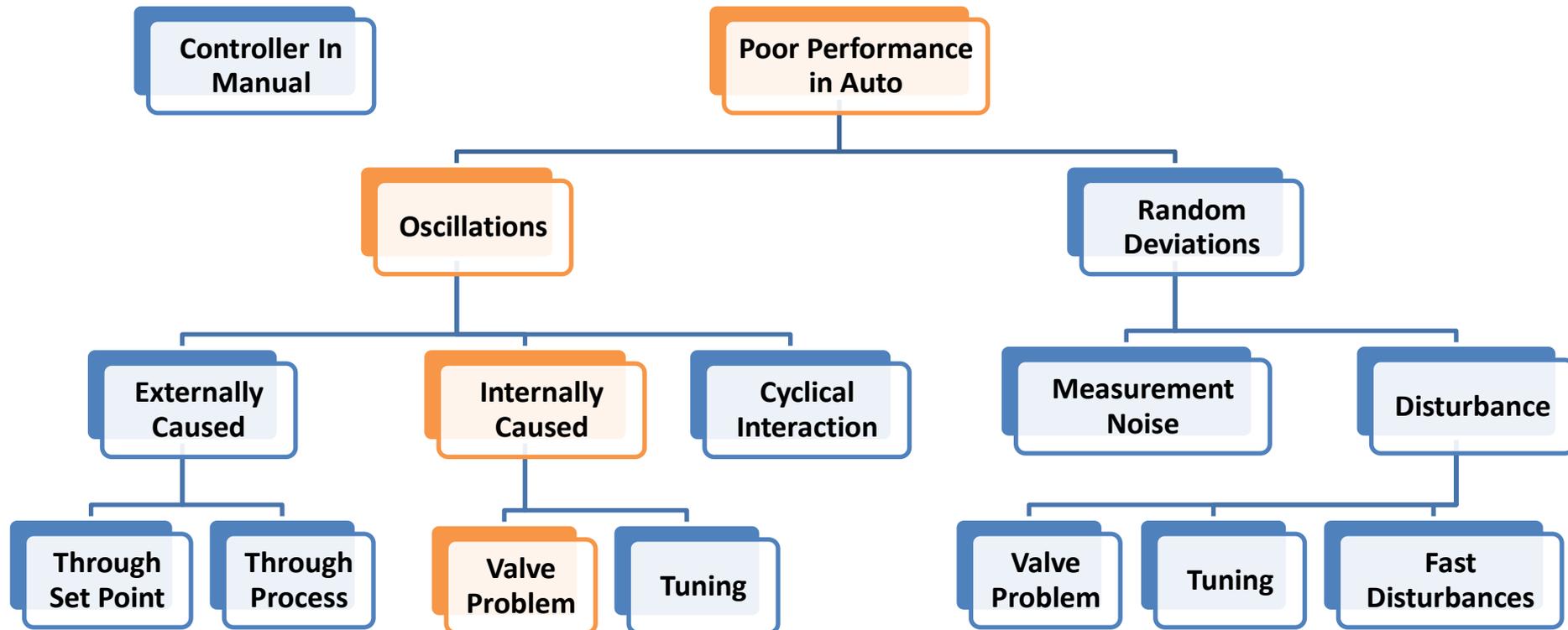


Interaction through Process

- ▶ Interactive process
 - Heat integration, recycle, etc.
- ▶ Oscillating loop elsewhere
- ▶ Affects other loops
- ▶ Interaction analysis tools
 - PAS, ExperTune, Matrikon
- ▶ P&ID and Process Historian
- ▶ Look for leading oscillation
- ▶ Look at shape of oscillation

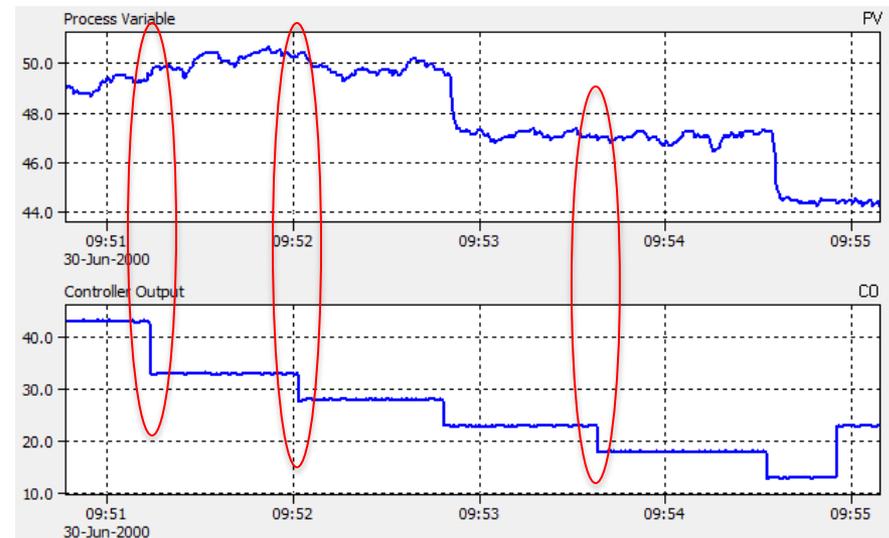
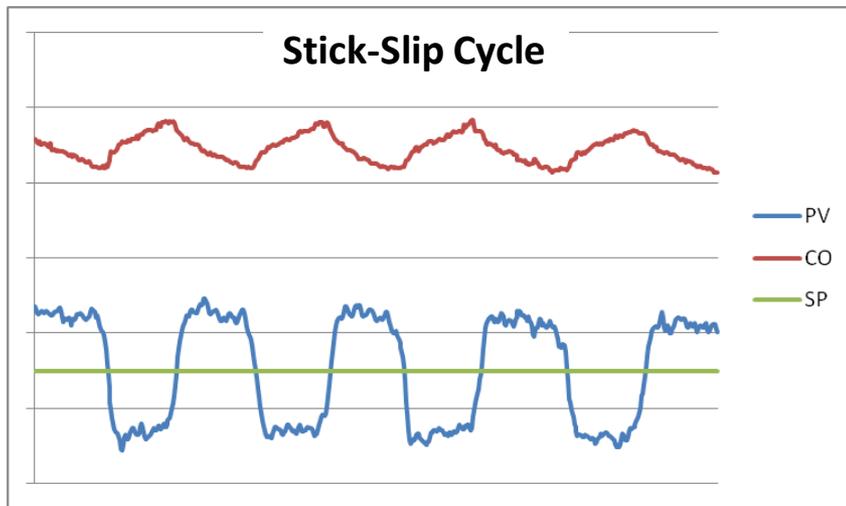


Problem Analysis



Stiction

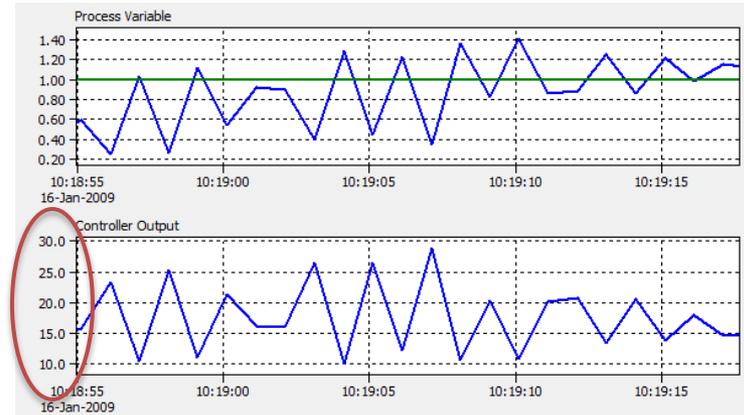
- ▶ Short for “Static Friction”
- ▶ Final control element is sticky
- ▶ Can cause a “stick-slip” cycle with loop in auto
- ▶ Stiction test: small controller output changes



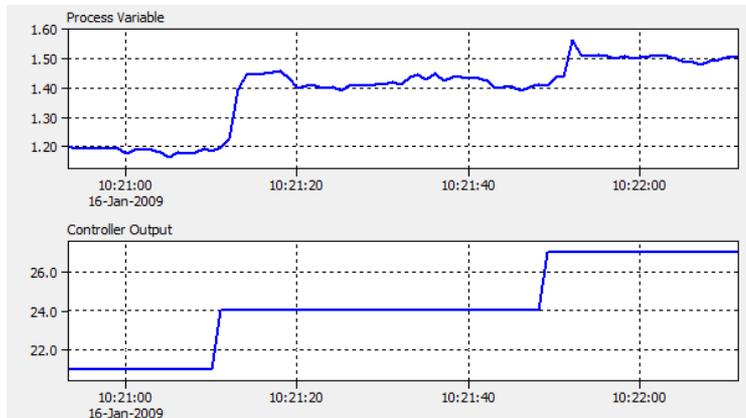
White water flow controller

Positioner Problem

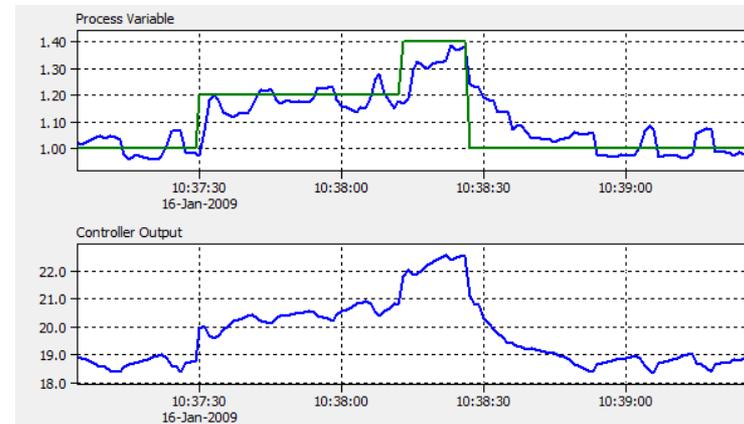
- ▶ Defective positioner
- ▶ Incorrectly tuned positioner
- ▶ Sticky valve
- ▶ Revealed through small step tests



HP Flare Scrubber Flow Control as found – oscillating severely



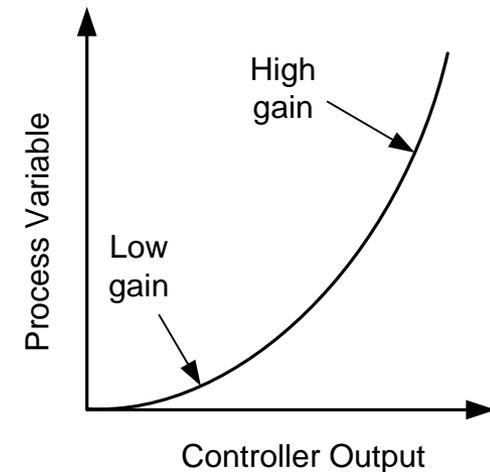
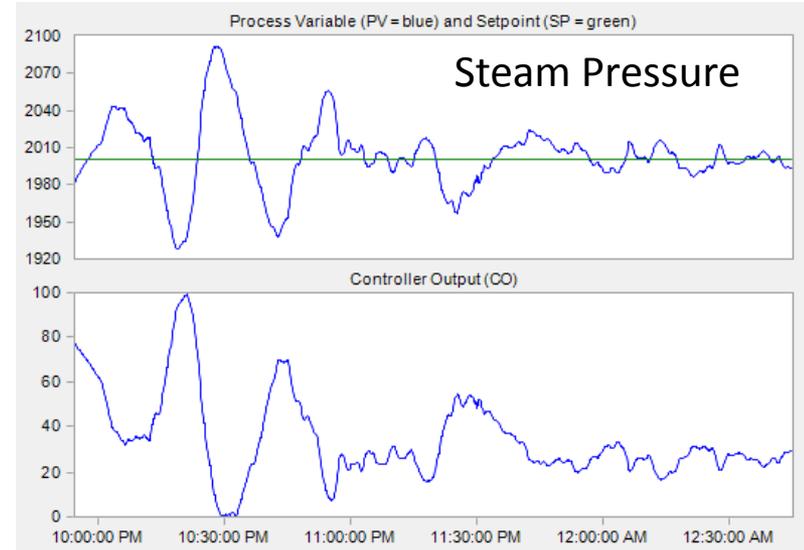
Step tests revealed positioner overshoot



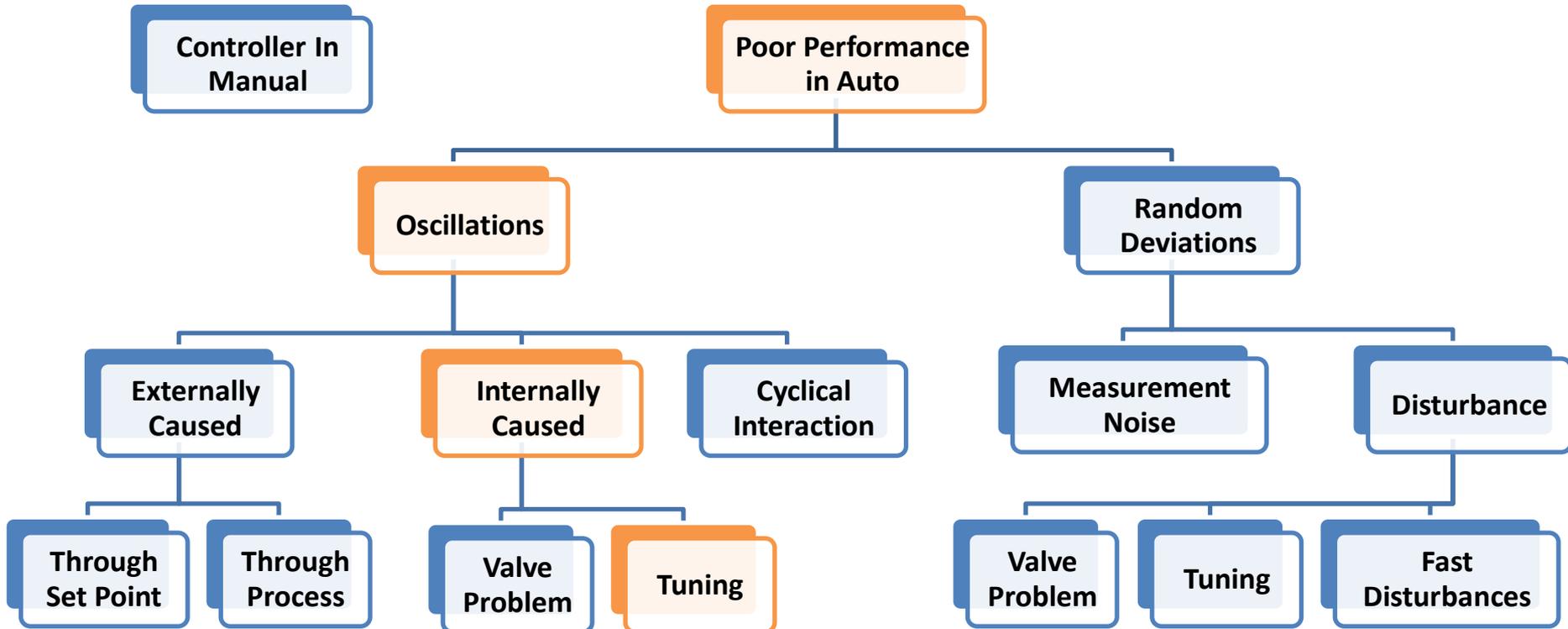
After tuning – still oscillating because of stiction, but much less

Nonlinearity

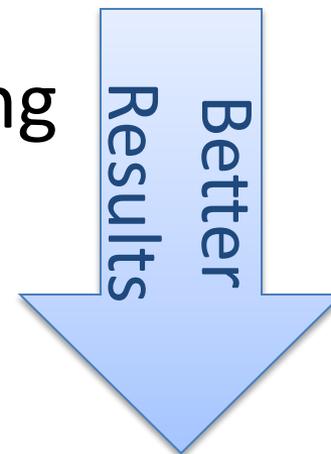
- ▶ Loop unstable under certain conditions
- ▶ Nonlinear valve characteristic
 - Plot Flow vs. % Open
 - Use characterizer
- ▶ Nonlinear process
 - Tune under different conditions
 - Use gain scheduling



Problem Analysis

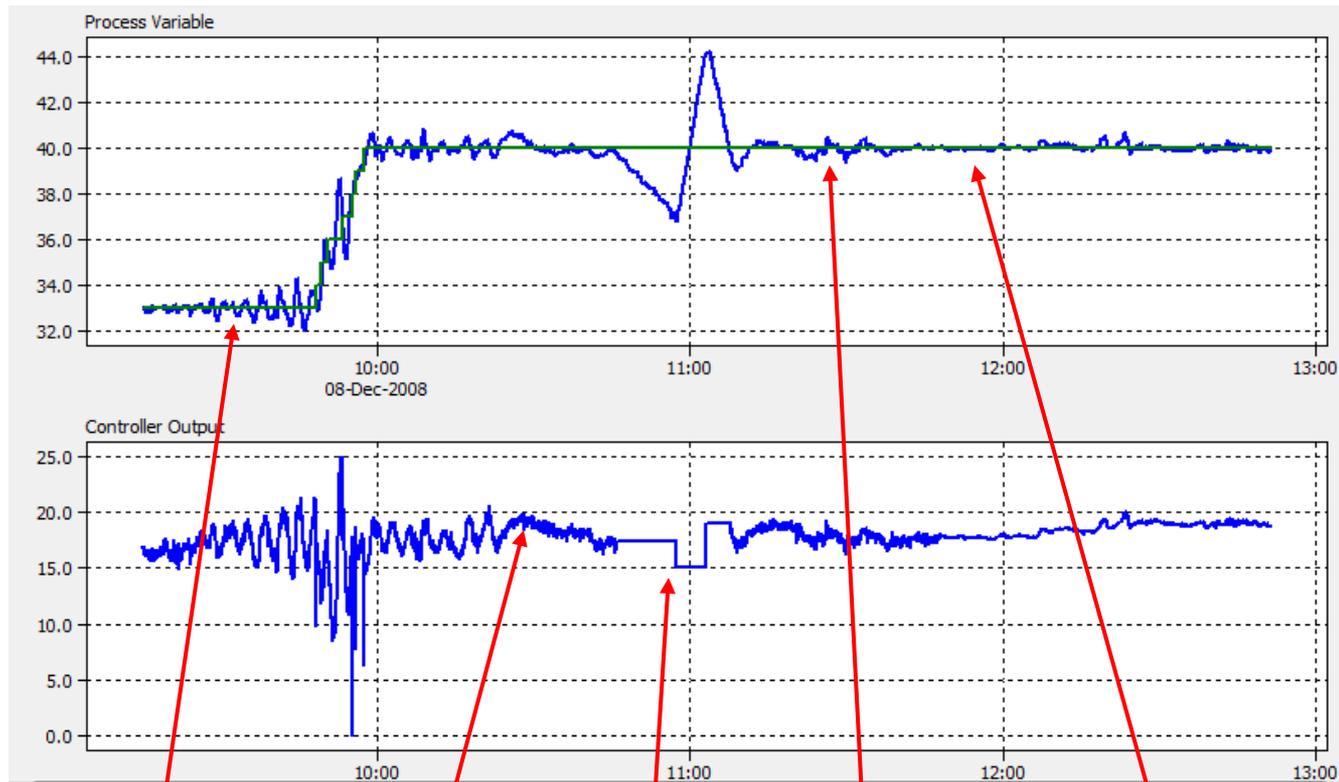


- ▶ Tune controller according to the process characteristics
- ▶ Tune controllers to meet control objective
- ▶ Trial-and-error tuning
- ▶ Tuning rules
- ▶ Tuning software



Tuning Example

► Oil-Gas Separator Level Control



As Found

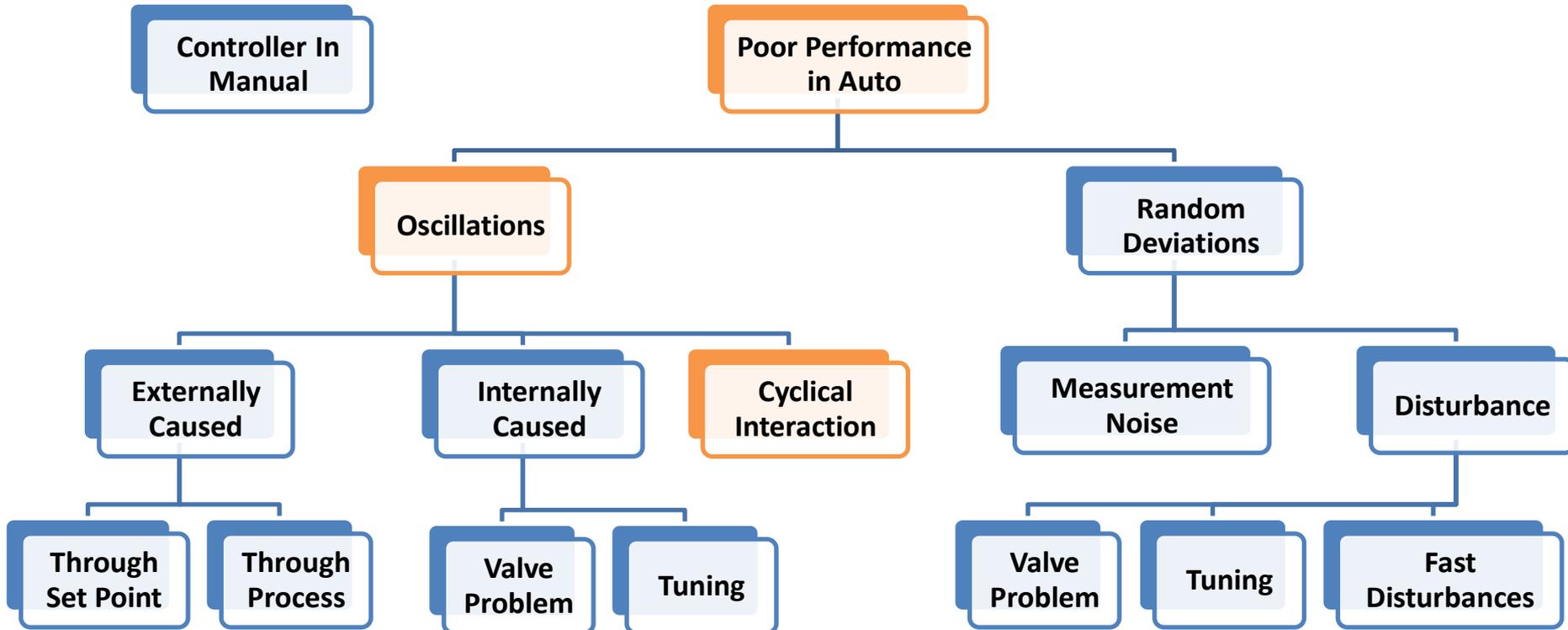
Quick
Stabilization

Step
Tests

After
Tuning

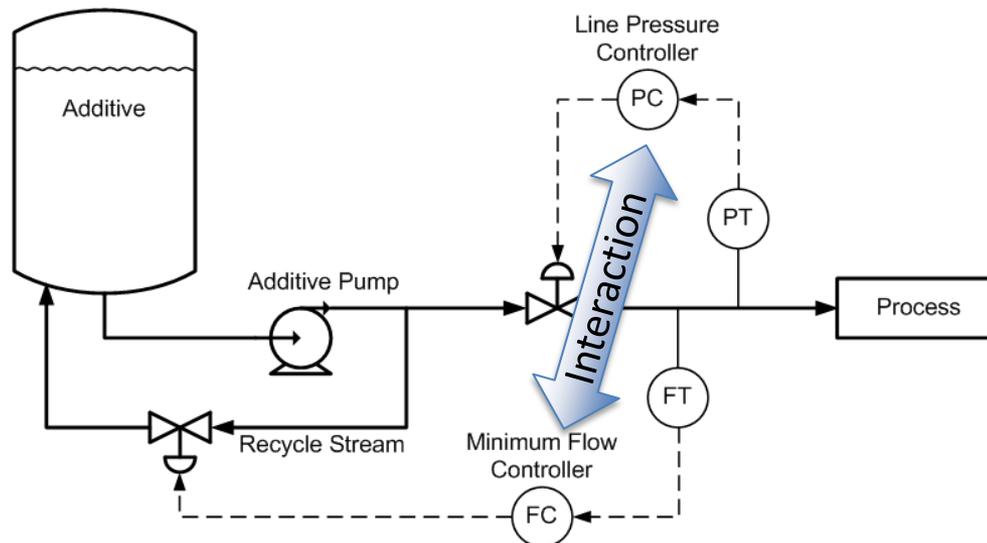
With PV Filter

Problem Analysis

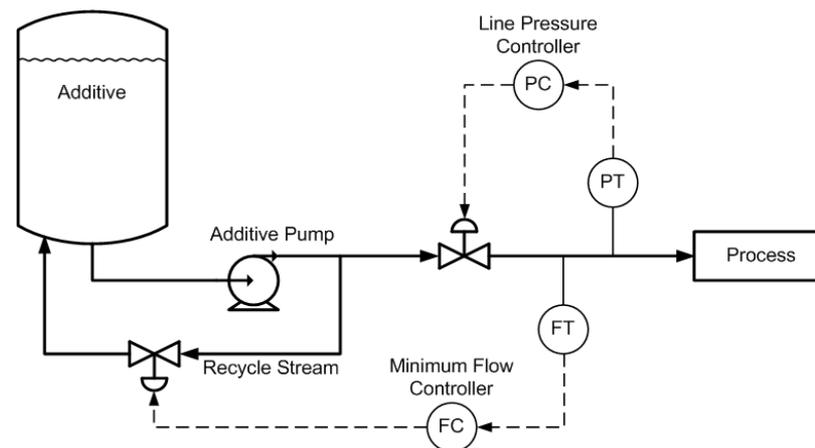


Cyclical Interaction

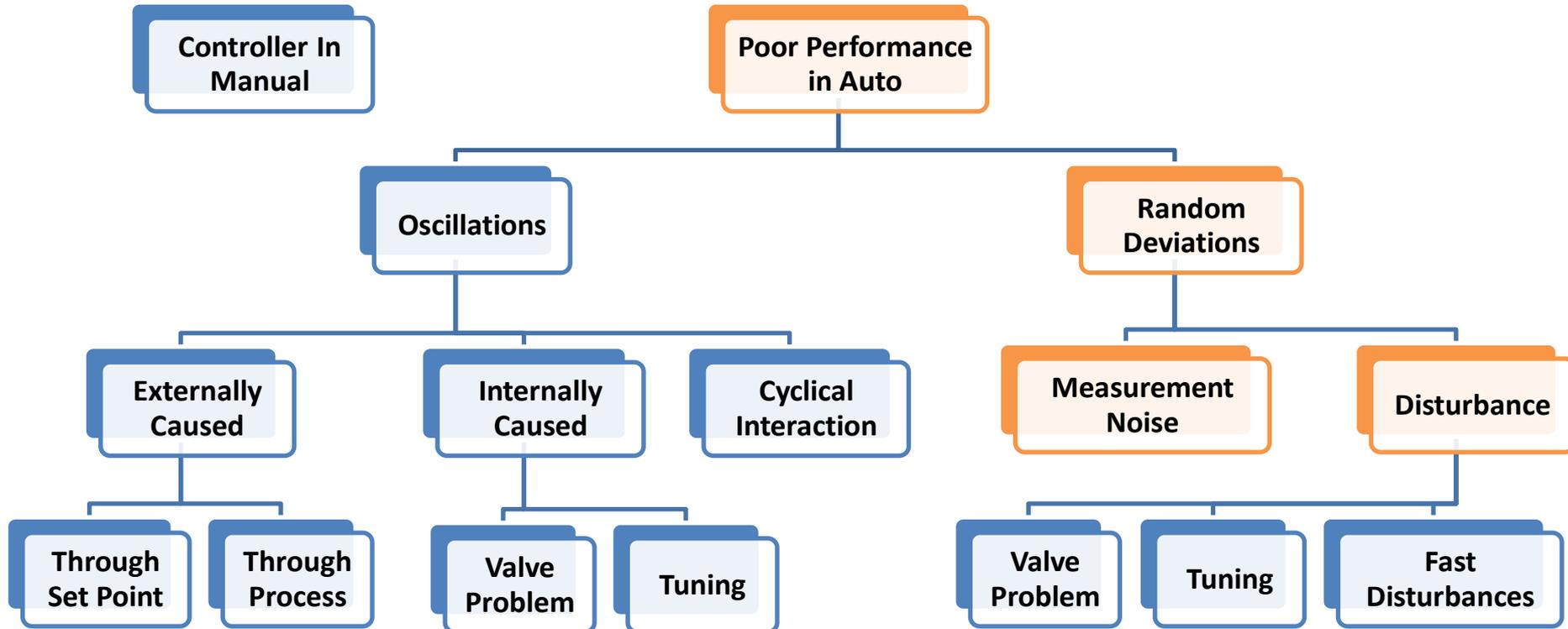
- ▶ Loops “fighting” with each other
- ▶ Continuous, interactive oscillations
 - Strong interaction
 - Similar dynamics
 - Aggressive tuning



- ▶ Dynamically separate loop response times
 - Tune most important loop for fast response
 - Tune interacting loop to respond 3 x slower
- ▶ Apply dynamic decoupling
 - Two cross-coupled feedforward controllers between loops
- ▶ Implement MPC

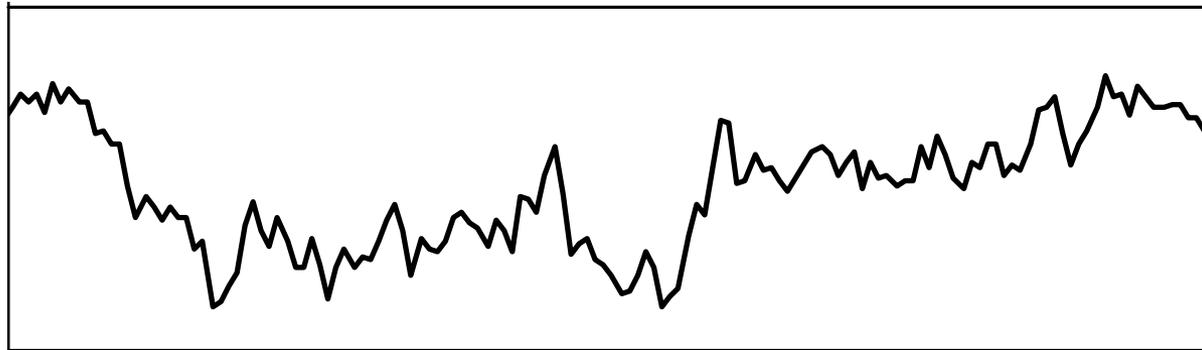


Problem Analysis

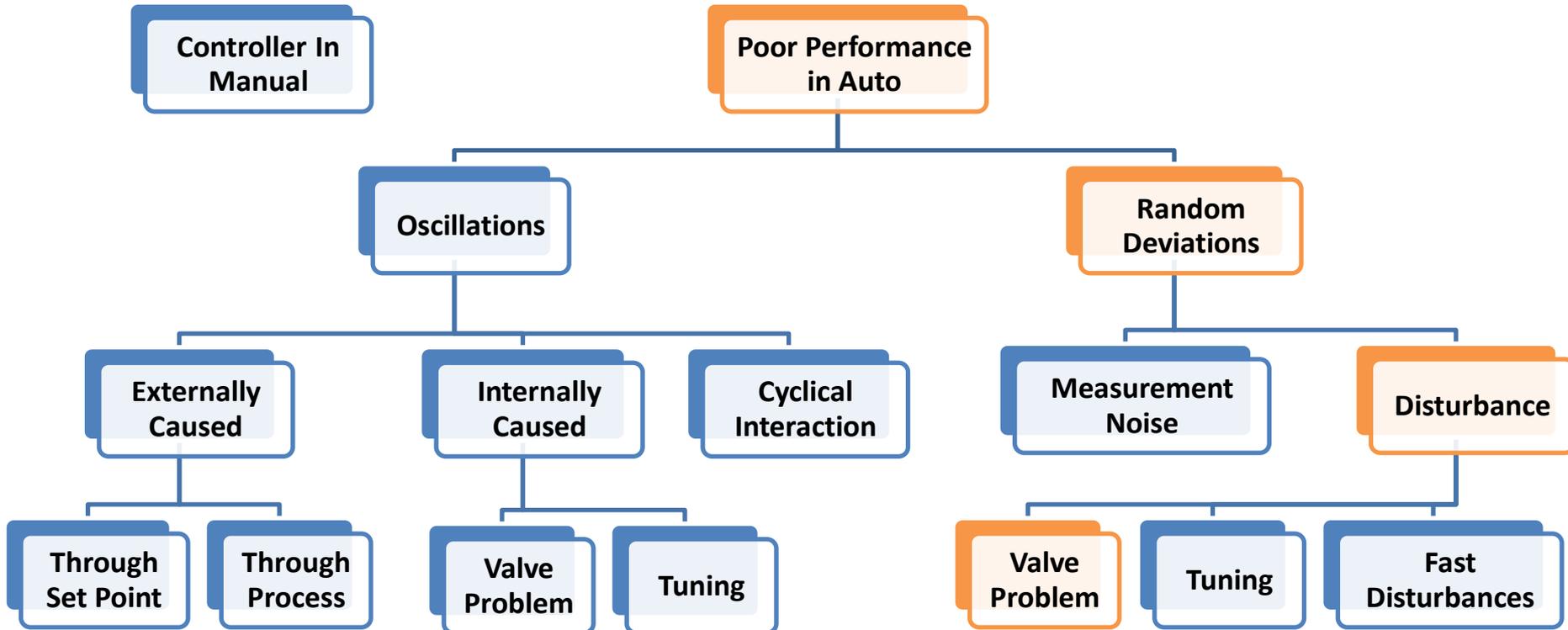


Noise or Disturbance

- ▶ Noise is fast changes
- ▶ Disturbances are longer in duration
- ▶ Can coexist
- ▶ Noise can be filtered

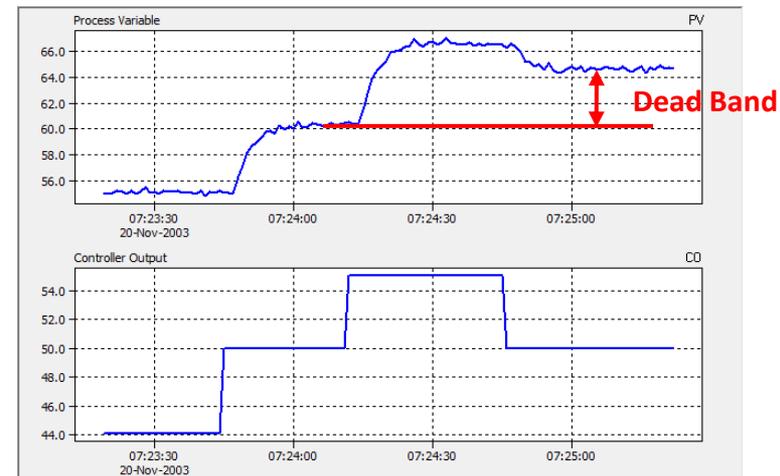
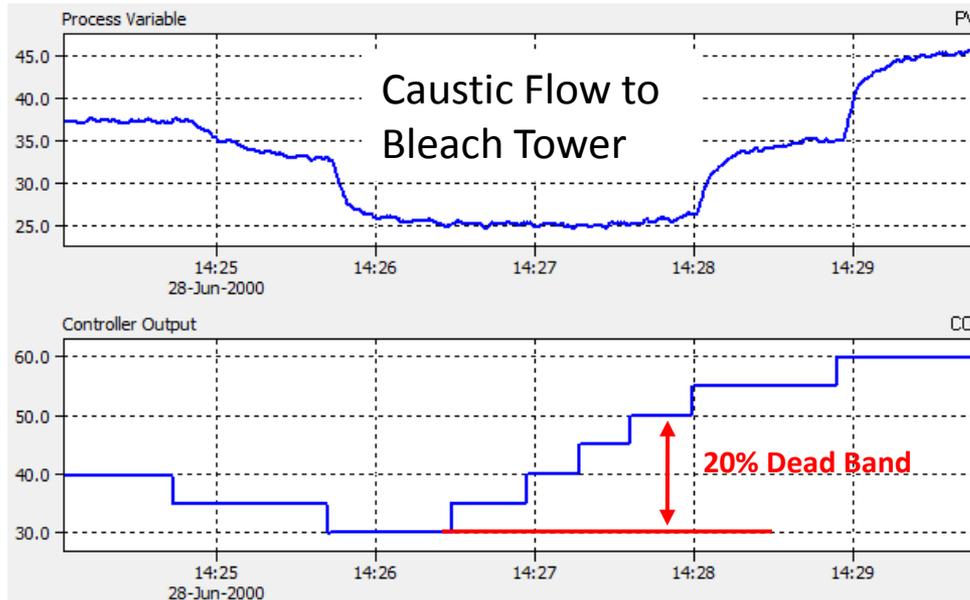


Problem Analysis



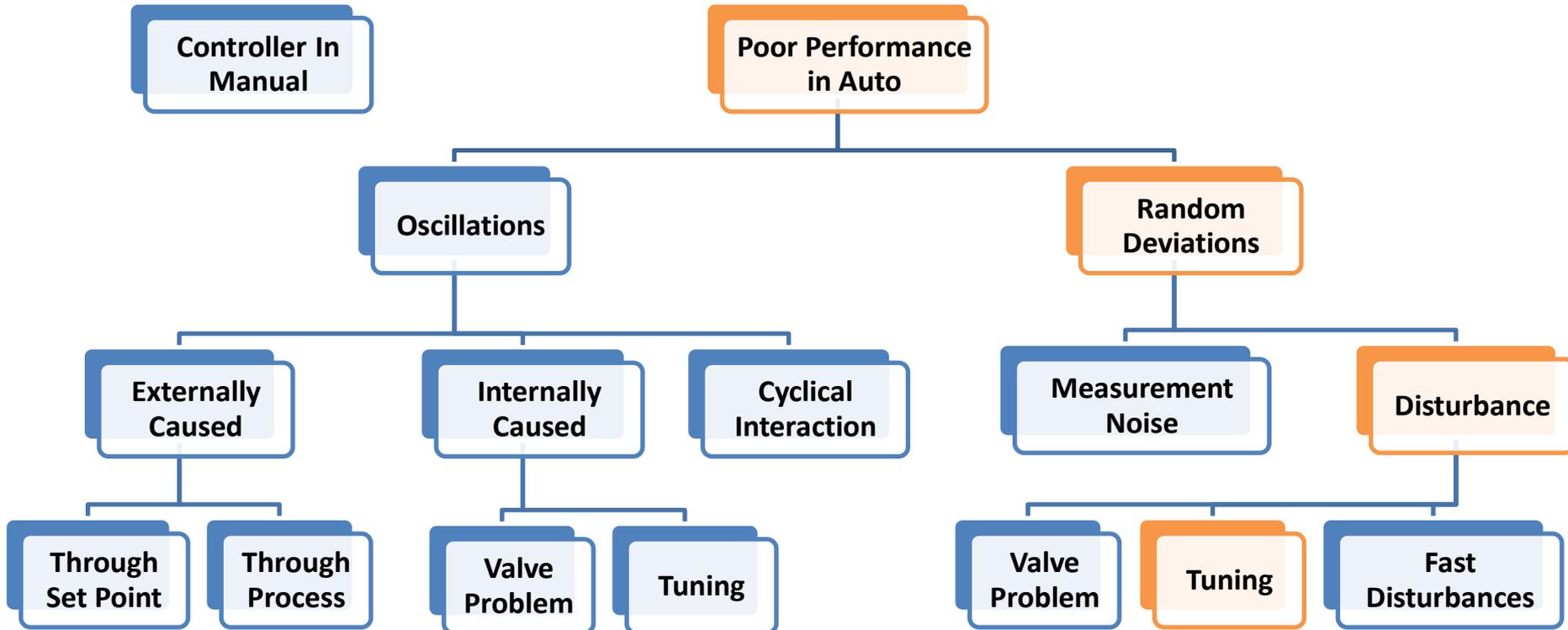
Dead Band (Hysteresis)

- ▶ Dead band between CO and PV
- ▶ Appears like sluggish control action
- ▶ Can result in very incorrect tuning calculations
- ▶ Dead-band test: 2 steps + 1 in opposite direction



Dead-Band Test

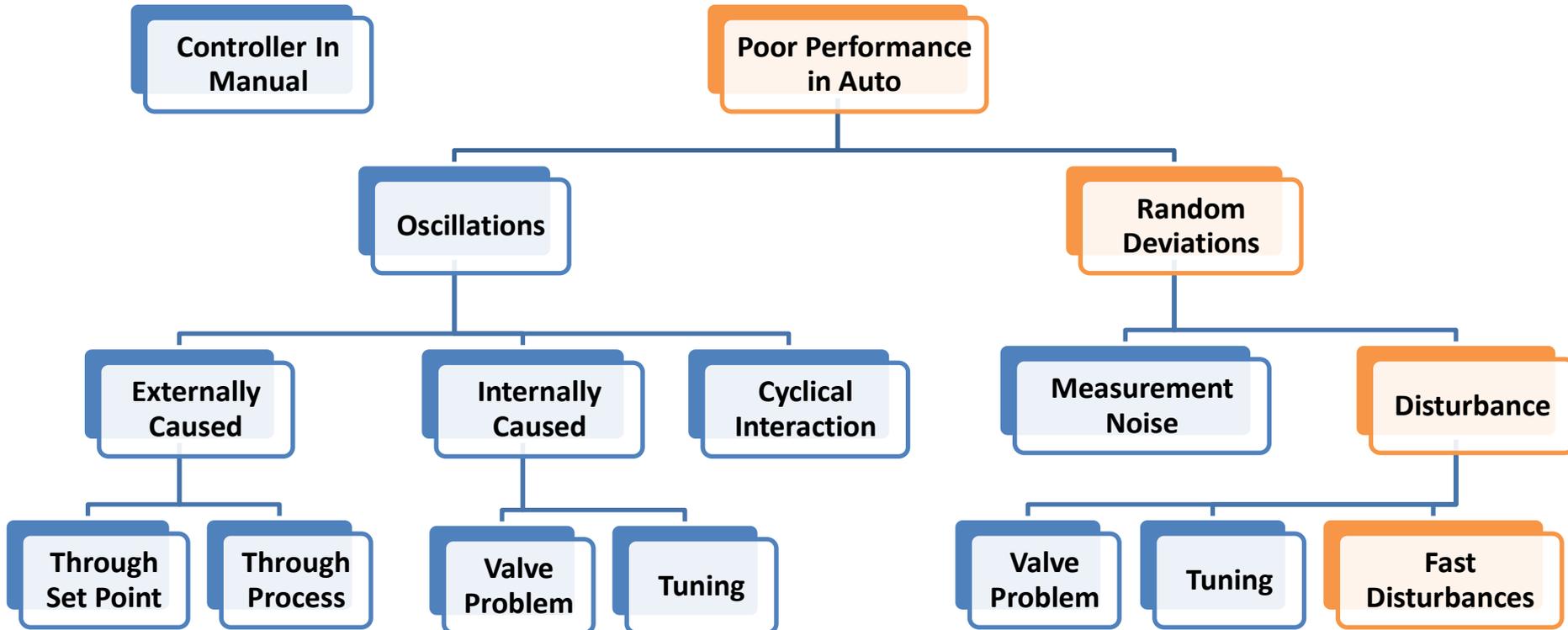
Problem Analysis



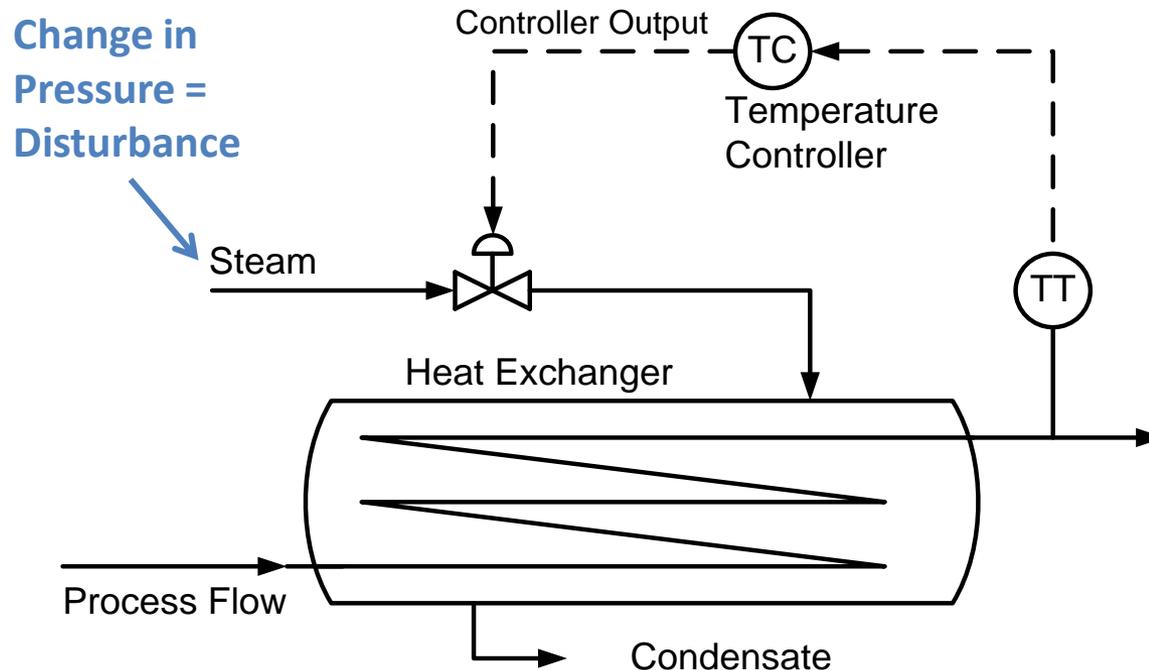
Tuning and Disturbance Rejection

- ▶ Previous comments about tuning apply
- ▶ Tuning (speed of response) has limits
 - Disturbance rejection
 - Settling time
- ▶ Limits mostly affected by dead time
- ▶ Other solutions are available

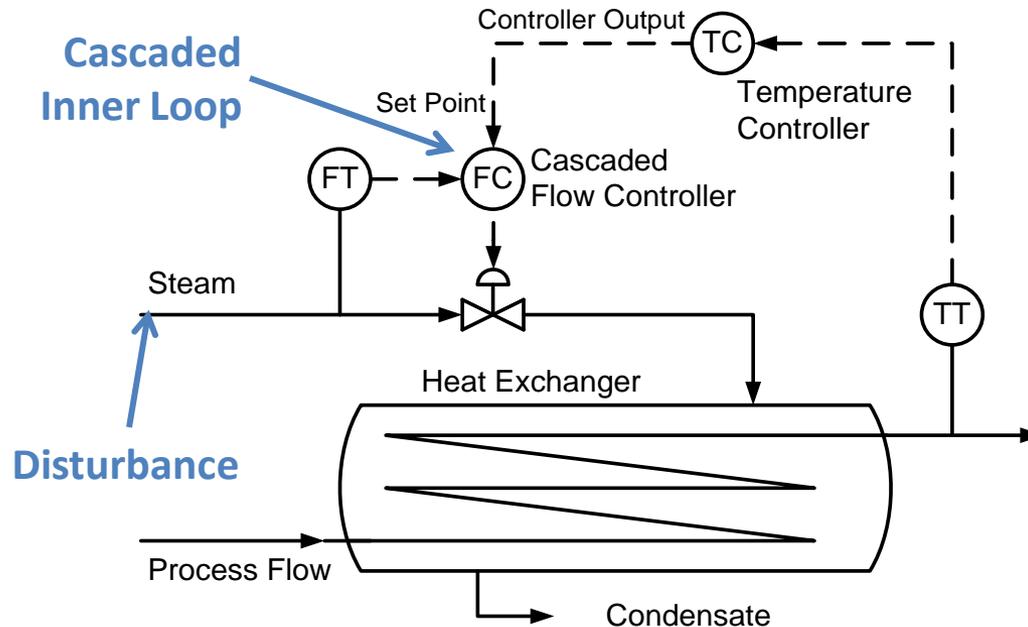
Problem Analysis



- ▶ Go unnoticed until PV has been affected
- ▶ E.g. steam pressure to heat exchanger

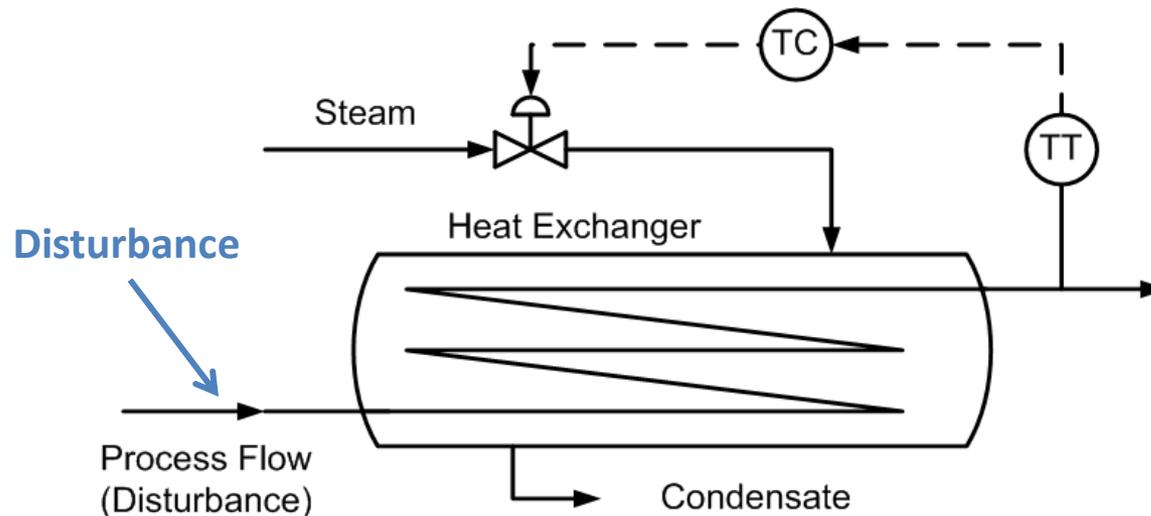


Solution: Cascade Control

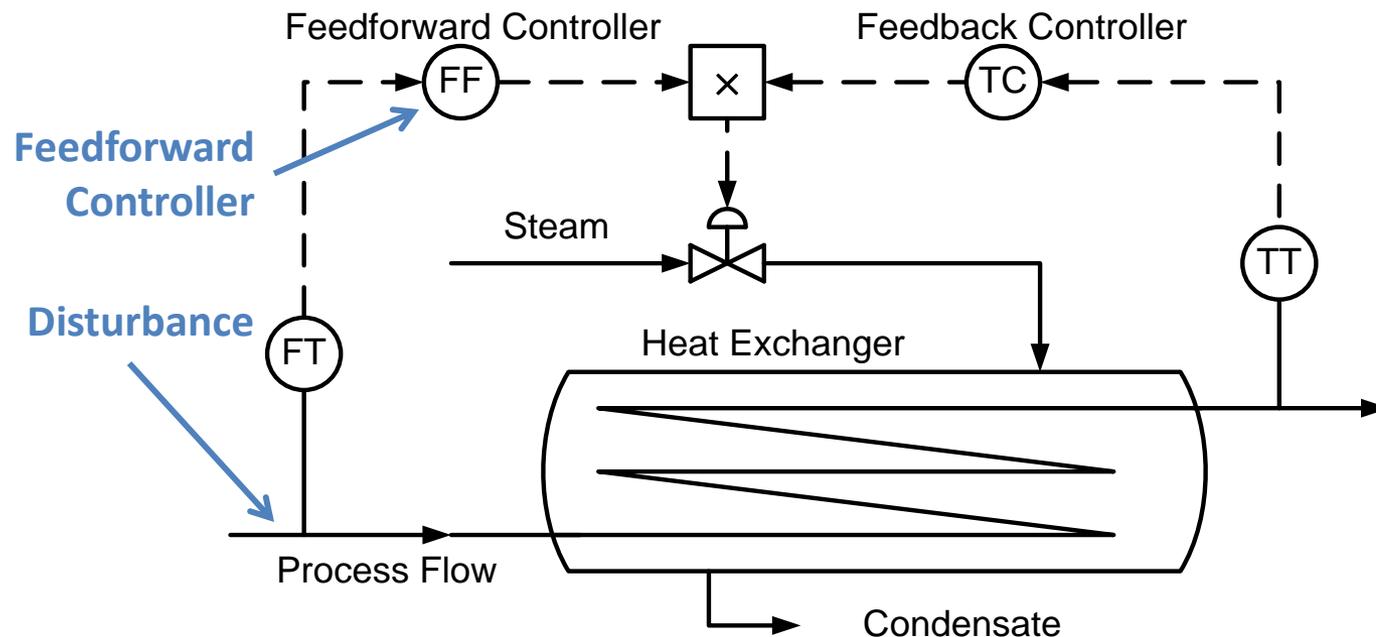


- ▶ Cascade control isolates control-side disturbances, nonlinearities, valve problems
- ▶ Good practice for any slow control loop manipulating a flow

- ▶ Go unnoticed until PV has been affected
- ▶ E.g. process flow through heat exchanger



- ▶ Use disturbance to drive control action
- ▶ Feedforward control action can cancel out effect of major disturbances



Summary

- ▶ Some poorly performing loops are a challenge to tune
- ▶ Realize that it might not be a tuning problem
- ▶ Do process tests to detect valve problems
- ▶ Valve problems require repairs, not tuning
- ▶ Tune from step test data using rules or software
- ▶ Know the limitations of tuning
- ▶ The problem may originate from outside the loop
- ▶ Eliminate variability at its source
- ▶ Enhance the control strategy where needed

Questions?